PATENT COOPERATION TREATY

PCT

REC'D 11 APR 2001

REPLACED BY INTERNATIONAL PRELIMINARY EXAMINATION REPORT

(PCT Article 36 and Rule 70)

Applicantle of a	gontla file reference	T					
Applicant's or agent's file reference FOR FURTHER AC		See Notification of Transmittal of International					
HL 71373/002			Tommany Examination Toport (Form Form Ex-410)				
	International application No.		day/month/year)	Priority date (day/month/year)			
PCT/GB00/0	0673	24/02/2000		04/03/1999			
International Pa C07C41/09	tent Classification (IPC) or na	tional classification and IP	C				
Applicant							
THOMAS SV	VAN & CO. LTD. et al.						
This international preliminary examination report has been and is transmitted to the applicant according to Article 36.			prepared by this Int	ernational Preliminary Examining Authority			
2. This REPORT consists of a total of Scheets, including this			s cover sheet.				
This report is also accompanied by ANNEXES, i.e. she been amended and are the basis for this report and/or (see Rule 70.16 and Section 607 of the Administrative			sheets containing re	ectifications made before this Authority			
These and	nexes consist of a total of	5 sheets.					
3. This repor	t contains indications rela	ting to the following iter	ns:				
l ⊠							
	Priority						
III			velty, inventive step	and industrial applicability			
	Lack of unity of invention						
	citations and explanation	ns suporting such state	egard to novelty, inve ement	entive step or industrial applicability;			
	Certain documents cite						
	Certain defects in the in						
VIII ⊠	Certain observations or	i the international applic	SLST A	WAILABLE COPY			
Date of submission of the demand			Date of completion of	this report			
20/09/2000			09.04.2001				
Name and mailing address of the international preliminary examining authority:			Authorized officer	SHOURS MILES			
European Patent Office							
D-80298 Munich Tel. +49 89 2399 - 0 Tx: 523656 epmu d			Lorenzo, M.J.				
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Form PCT/IPEA/40	09 (cover sheet) (January 19	94)		AVAILABLE COPY			

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No. PCT/GB00/00673

	P.	sis of the report	•							
	Wit the	th regard to the let receiving Office in d are not annexed t scription, pages:	Article 14	are referred	d to in thi	s report as	"origina	rnished to ally filed"		
		4, 6-15 5a	received ou	14.0	3.01	filed	with	leller	of	12.03
	Cla	Claims, No.: 1-16 received on 14.03.01 filed with letter of 12.09								
	1-1	6	received on	14. O	3.01	filed	with	letter	of	12.03
	Dra	awings, sheets:								
	1/1		as originally filed							·
2.	. With regard to the language , all the elements marked above were available or turnished to this Authority in language in which the international application was filed, unless otherwise indicated under this item.						ity in the			
	The	ese elements were a	available or furnished	to this Aut	hority in th	e following	languag	e: , which	n is:	
		the language of a	translation furnished f	or the purp	oses of th	ne internatio	onal sear	ch (under f	Rule 23	.1(b)).
		the language of a 55.2 and/or 55.3).	translation furnished f	or the purp	ooses of in	iternational	prelimin	ary examin	ation (u	ınder Rule
3.	Witl inte	With regard to any nucleotide and/or amino acid sequence disclosed in the international application, the international preliminary examination was carried out on the basis of the sequence listing:				the				
		Contained in the international application in written form.								
		☐ filed together with the international application in computer readable form.								
		☐ furnished subsequently to this Authority in written form.								
		furnished subsequently to this Authority in computer readable form.								
		The statement that the subsequently furnished written sequence listing does not go beyond the disclosure in the international application as filed has been furnished.								
		The statement that the information recorded in computer readable form is identical to the written sequence listing has been furnished.								
4.	The	amendments have	amendments have resulted in the cancellation of:							
		☐ the description, pages:								
		the claims,	Nos.:							
							1	COPY	,	

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INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No. PCT/GB00/00673

	the drawings,	sheets:
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5. A This report has been established as if (some of) the amendments had not been made, since they have been considered to go beyond the disclosure as filed (Rule 70.2(c)):

(Any replacement sheet containing such amendments must be referred to under item 1 and annexed to this report.)

see separate sheet

- 6. Additional observations, if necessary:
- V. Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement
- 1. Statement

Novelty (N)

Yes: No: Claims

Claims 1-16

Inventive step (IS)

Yes:

Claims

No:

Claims 1-16

Industrial applicability (IA)

Yes: Claims 1-16

No: Claims

2. Citations and explanations see separate sheet

VI. Certain documents cited

1. Certain published documents (Rule 70.10)

and / or

2. Non-written disclosures (Rule 70.9)

see separate sheet

VII. Certain defects in the international application

The following defects in the form or contents of the international application have been noted: see separate sheet

VIII. Certain observations on the international application

The following observations on the clarity of the claims, description, and drawings or on the question whether the claims are fully supported by the description, are made:

see separate sheet

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Basis of the report

The amendments submitted by the applicant with his letter dated 12.03.01 do not fulfil the requirements of Article 19(2) PCT. The amendments on claim 1 and on page 5 of the description changing "under supercritical or near-critical conditions" by "under supercritical or near-critical conditions for the fluid that is acting as solvent" are considered to go beyond the disclosure as filed (Rule 70.2(c)). Therefore, the establishment of opinion with regard to novelty, inventive step and industrial applicability is based on the application as originally filed.

Re Item V

Reasoned statement under Rule 66.2(a)(ii) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

D1: US-A-5 831 116

The present application relates to a method for producing ether, acetal, ketal or alkene derivatives which comprises reacting an alcohol in the presence of a heterogeneous acid catalyst under supercritical or near critical conditions.

The closest prior art, document D1, discloses a method for partially oxidising alcohols which comprises a)introducing into a reactor unit containing a bed of solid acid catalyst (Lewis acid), an alcohol, oxygen and a supercritical fluid (such as CO2 or N2) mobile phase; and b)partially oxidising the alcohol to its corresponding ether, aldehyde, ester or acid, wherein the operating pressure and temperature are greater than the critical point pressure and temperatures of the mixture of alcohol, oxygen and the supercritical fluid.

The disclosure of D1 anticipates thus the subject-matter of claims 1-16 of the present application which are, therefore, not novel according to Article 33(2) PCT. The objection raised in the previous communication against the subject-matter of the application for lack of novelty is, despite the arguments brought forward in the Applicant's letter of reply, maintained.

Re It m Vi

Certain documents cited

Although the document J. Am. Chem. Soc. published on 11.06.99 is not considered to be part of the prior art in the sense of Rule 64.1 PCT for the purposes of Articles 33(2) and (3) PCT, this document (see abstract and tables 2-6) would anticipate the subject-matter of the claims of the present application if the priority date of the latter is not valid. This document could become very relevant to assess the patentability of the present application when it enters the national/regional phase. No check has been made as to whether the priority of the present application has been validly claimed.

Re Item VII

Certain defects in the international application

- 1. Contrary to the requirements of Rule 5.1(a)(ii) PCT, the relevant background art disclosed in the document D1 is not mentioned in the description, nor is this document identified therein.
- 2. The units of pressure "atm" employed in examples 4-8 are not additionally expressed in terms of the units stipulated by Rule 10.1/(a)/and/(b) PCT.

Re Item VIII

Certain observations on the international application

- Claims 11 and 15 do not meet the requirements of Article 6 PCT in that the matter 1. for which protection is sought is not defined. The claims attempt to define the subjectmatter in terms of the result to be achieved. In this instance, such a formulation is not allowable because it appears possible to define the subject-matter in more concrete terms, viz. in terms of how the effect is to be achieved.
- 2. Features introduced by "preferred" in claim 2 have no limiting effect on the scope of the claim (see PCT Guidelines, C-IV, 4.6). The presence of such non-limiting features is however detrimental to the conciseness of the claim, contrary to Art. 6 PCT.

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One consequence of using the heterogeneous catalyst is that there is no need for complicated separation procedures to liberate the product from the reaction mixture and catalyst. This represents quite a benefit in terms of both the time savings and cost savings of the present invention.

We have thus found that it is possible by using a combination of supercritical fluids and a heterogeneous catalyst (e.g. the Deloxan ASP catalyst from Degussa or Acidic Amberlyst resin from Rohm and Haas) in a continuous flow reactor to carry out a number of reactions rapidly and cleanly. These reactions can often be performed in high yield and take place under near-critical or supercritical conditions.

According to the present invention, there is provided A process in which a hydroxyl-substituted organic compound selected from the formulae R1CH2OH, R^1R^2CHOH and $R^1R^2R^3COH$ is exposed, optionally in the presence of one or more further organic compounds selected from second hydroxyl-substituted organic compounds of the formulae R4CH2OH, R5R6CHOH, and R7R8R9COH. and carbonyl compounds of the formula $R^{10}R^{11}CO$, to a heterogeneous catalyst which is able to provide a source of acid in a continuous flow reactor under supercritical conditions or at near-critical conditions for the fluid that is acting as solvent, with the result that an ether is formed from two hydroxylsubstituted organic compound molecules in a dehydration reaction, an acetal or ketal is formed by reaction between a hydroxyl-substituted organic compound molecule and a molecule of a said carbonyl compound and an alkene product is produced by dehydration of a single hydroxyl-substituted organic compound molecule, wherein the conditions of temperature, pressure, and flow rate are controlled according to the product to be obtained, and wherein each of R1 to R11 is independently

selected from: hydrogen or hydroxyl; an optionally substituted alkyl, alkenyl, alkynyl, aralkyl, cycloalkyl, cycloalkenyl, or aryl; or a heterocyclic group.

Aliphatic and aromatic alcohols are preferred because they give cleaner reactions, with aliphatic alcohols being most preferred on the grounds of ease of use and lower occurrence of side products.

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Claims

- A process in which a hydroxyl-substituted organic compound selected from the formulae R1CH2OH, R^1R^2CHOH and $R^1R^2R^3COH$ is exposed, optionally in the 5 presence of one or more further organic compounds selected from second hydroxyl-substituted organic compounds of the formulae R4CH2OH, R5R6CHOH, and R7R8R9COH and carbonyl compounds of the formula R10R11CO, to a heterogeneous catalyst which is able to provide a source of acid in a continuous flow reactor under 10 supercritical conditions or at near-critical conditions for the fluid that is acting as solvent, with the result that an ether is formed from two hydroxylsubstituted organic compound molecules in a dehydration reaction, an acetal or ketal is formed by reaction 15 between a hydroxyl-substituted organic compound molecule and a molecule of a said carbonyl compound and an alkene product is produced by dehydration of a single hydroxyl-substituted organic compound molecule, wherein the conditions of temperature, pressure, and 20 flow rate are controlled according to the product to be obtained, and wherein each of R1 to R11 is independently selected from: hydrogen or hydroxyl; an optionally substituted alkyl, alkenyl, alkynyl, aralkyl, 25 cycloalkyl, cycloalkenyl, or aryl; or a heterocyclic group.
 - 2. A process according to claim 1, wherein each of R¹ to R¹¹ when present is an optionally substituted alkyl group.
 - 3. A process according to claim 2, wherein each of the alkyl groups independently contains not more than 10 carbon atoms in the carbon chain (excluding optional substituents if present).

- 4. A process according to claim 1, 2 or 3, wherein the total number of alcohol groups within the organic compound does not exceed three.
- 5. A process according to any preceding claim, wherein the reaction is performed under supercritical conditions.
- 6. A process according to any preceding claim,
 wherein the organic compound of formula R¹CH2OH, R¹R²CHOH
 or R¹R²R³COH, and optionally one or more of the
 compounds of formulae R⁴CH2OH, R⁵R6CHOH, R²R8R9COH
 or R¹0R¹¹CO, is dissolved in a fluid selected from:
 carbon dioxide, propane, an alkene, an alkyne,
 hydrocarbon, halocarbon, nitrogen, or a mixture of any
 of these.
- 7. A process according to any one of claims 1 to 5, wherein the organic compound is the supercritical or near-critical fluid.
 - 8. A process according to any preceding claim, wherein the catalyst is selected from: zeolites, metal oxides, molecular sieves, clays, or sulfonic acid derivatives.
 - 9. A process according to claim 8, wherein the catalyst is supported on an inert carrier.
- 10. A process according to claim 8 or 9, wherein the catalyst includes a promoter.
- 11. A process according to any of claims 8, 9 or 10, wherein the acidity of the catalyst is provided by a sulfonic acid group.

- 12. A process according to any preceding claim, wherein the reactant molecules are aliphatic and/or aromatic alcohols.
- 5 13. A process according to any preceding claim, in which the product is an ether.
 - 14. A process according to claim 13, in which the reactant(s) and the product are straight-chain n-alkyl molecules.
 - 15. A process according to claim 11 or 12, wherein an aliphatic alcohol is converted into an alkene.

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16. A process according to any preceding claim, in which the reactant(s) form a single homogeneous phase.

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One consequence of using the heterogeneous catalyst is that there is no need for complicated separation procedures to liberate the product from the reaction mixture and catalyst. This represents quite a benefit in terms of both the time savings and cost savings of the present invention.

We have thus found that it is possible by using a combination of supercritical fluids and a heterogeneous catalyst (e.g. the Deloxan ASP catalyst from Degussa or Acidic Amberlyst resin from Rohm and Haas) in a continuous flow reactor to carry out a number of reactions rapidly and cleanly. These reactions can often be performed in high yield and take place under near-critical or supercritical conditions.

According to the present invention, there is provided a process in which an organic compound having the formula R1CH2OH, R1R2CHOH, or R1R2R3COH is exposed, optionally in the presence of one or more further organic compounds having the formula R4CH,OH, R5R6CHOH, R'R'R'COH or R''R''CO, to a heterogenous catalyst which is able to provide a source of acid in a continuous flow reactor under supercritical or near-critical conditions with the result that an ether, acetal, ketal or alkene product is formed, wherein the conditions of temperature, pressure, and flow rate are independently controlled, and wherein each of R1 to R11 is independently selected from: hydrogen, hydroxyl, or an optionally substituted alkyl, alkenyl, alkynyl, aralkyl, cycloalkyl, cycloalkenyl, aryl or heterocyclic group.

Aliphatic and aromatic alcohols are preferred because they give cleaner reactions, with aliphatic alcohols being most preferred on the grounds of ease of use and lower occurrence of side products.

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Claims

- 1. A process in which an organic compound having the formula R1CH2OH, R1R2CHOH or R1R2R3COH is exposed, optionally in the presence of one or more further organic compounds having the formulae R4CH2OH, R5R6CHOH, $\mbox{R}^{7}\mbox{R}^{8}\mbox{R}^{9}\mbox{COH}$ or $\mbox{R}^{10}\mbox{R}^{11}\mbox{CO},$ to a heterogeneous catalyst which is able to provide a source of acid in a continuous flow reactor under supercritical or near-critical conditions with the result that an ether, acetal, ketal or alkene product is formed, wherein the conditions of temperature, pressure, and flow rate are independently controlled, and wherein each of R1 to R11 is independently selected from: hydrogen or hydroxyl; an optionally substituted alkyl, alkenyl, alkynyl, aralkyl, cycloalkyl, cycloalkenyl, or aryl; or a heterocyclic group.
 - 2. A process according to claim 1, wherein each of R^1 to R^{11} when present is an optionally substituted alkyl group, preferably each of the alkyl groups independently containing not more than 10 carbon atoms in the carbon chain (excluding optional substituents if present).
 - 3. A process according to claim 1 or 2, wherein the total number of alcohol groups within the organic compound does not exceed three.
 - 4. A process according to claim 1, 2 or 3, wherein the reaction is performed under supercritical conditions.
- 5. A process according to any preceding claim,
 wherein the organic compound of formula R¹CH2OH, R¹R²CHOH
 or R¹R²R³COH, and optionally one or more of the
 compounds of formulae R⁴CH2OH, R⁵R6CHOH, R7R8R9COH
 or R¹OR¹¹CO, is dissolved in a fluid selected from:
 carbon dioxide, propane, an alkene, an alkyne,
 hydrocarbon, halocarbon, nitrogen, or a mixture of any
 of these.

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- 6. A process according to claim 1, 2, 3 or 4, wherein the organic compound is the supercritical or near-critical fluid.
- 7. A process according to any preceding claim, wherein the catalyst is selected from: zeolites, metal oxides, molecular sieves, clays, or sulfonic acid derivatives.
 - 8. A process according to claim 7, wherein the catalyst is supported on an inert carrier.
- 9. A process according to claim 7 or 8, wherein the catalyst includes a promoter.
 - 10. A process according to any of claims 7, 8 or 9, wherein the acidity of the catalyst is provided by a sulfonic acid group.
- 11. A process according to any preceding claim, wherein the reaction conditions are controlled in such a way that the products are selectively formed in high yield with insignificant rearrangement.
 - 12. A process according to claim 11, wherein the reactant molecules are aliphatic and/or aromatic alcohols, preferably aliphatic alcohols.
 - 13. A process according to any preceding claim, in which the product is an ether.
- 14. A process according to claim 13, in which the reactant(s) and the product are straight-chain n-alkyl molecules.
 - 15. A process according to claim 11 or 12, wherein the reaction conditions can be controlled in such a way that a particular alcohol is converted into an alkene in preference to an ether.
 - 16. A process according to any preceding claim, in which the reactant(s) form a single homogeneous phase.

